

# Chapter 1 - Chemical Process Diagrams



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Spring, 2012

CHE 4101-Plant Design

**The most effective way of communicating information about a process is through the use of flow diagrams.**

Cyber Classroom

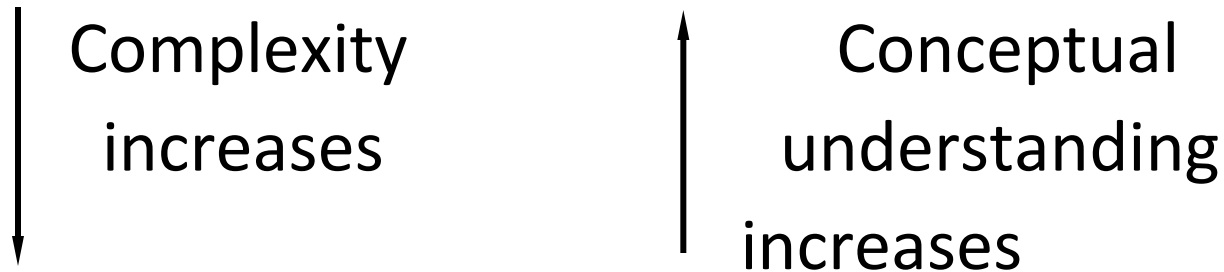
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# Outline

- Flow Diagrams
  - Block Flow Diagrams (BFD)
  - Process Flow Diagrams (PFD)
  - Piping and Instrument Diagrams (P&ID)
- Other common diagrams
- 3-D plant layout diagrams

# 3 Levels of Diagram

- Block Flow Diagram (BFD)
- Process Flow Diagram (PFD)
- Piping and Instrumentation Diagram (P&ID) – often referred to as Mechanical Flow Diagram



As chemical engineers, we are most familiar with BFD and PFD.

# The Block Flow Diagram (BFD)

- BFD shows overall processing picture of a chemical complex
  - Flow of raw materials and products may be included on a BFD
  - BFD is a superficial view of facility – Ch E information is missing

# Block Flow Diagrams (BFD)

- Emphasis not on details regarding blocks; focus on flow of streams through process.
- Conventions:
  - Operations shown by blocks
  - Major flow lines shown with arrows giving flow direction
  - Flow goes from left to right whenever possible
  - Light streams toward top, heavy streams toward bottom
  - Critical information unique to the process supplied (i.e., reaction stoichiometry, conversion)
  - Avoid crossing lines; horizontal continuous, vertical broken.
  - Simplified material balance (overall)

# Definitions of BFD

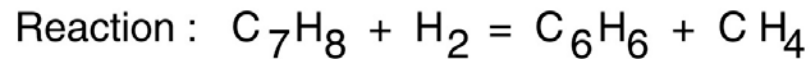
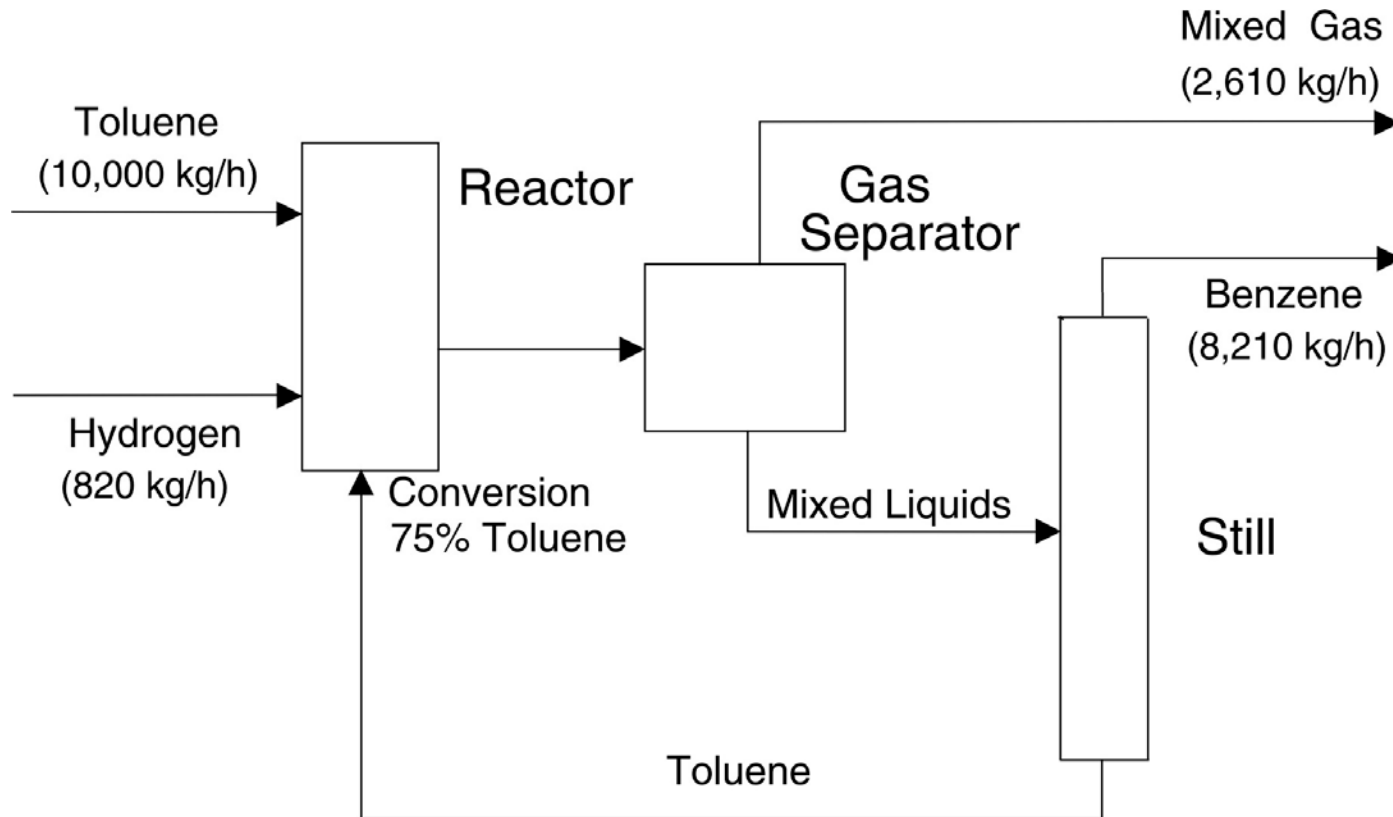
- Block Flow Process Diagram
  - Figure 1.1
  - Similar to sketches in material and energy balances

# Definitions of BFD

- Block Flow Plant Diagram
  - Figure 1.2
  - Gives a general view of a large complex plant



# The Block Flow Process Diagram



# The Block Flow Plant Diagram

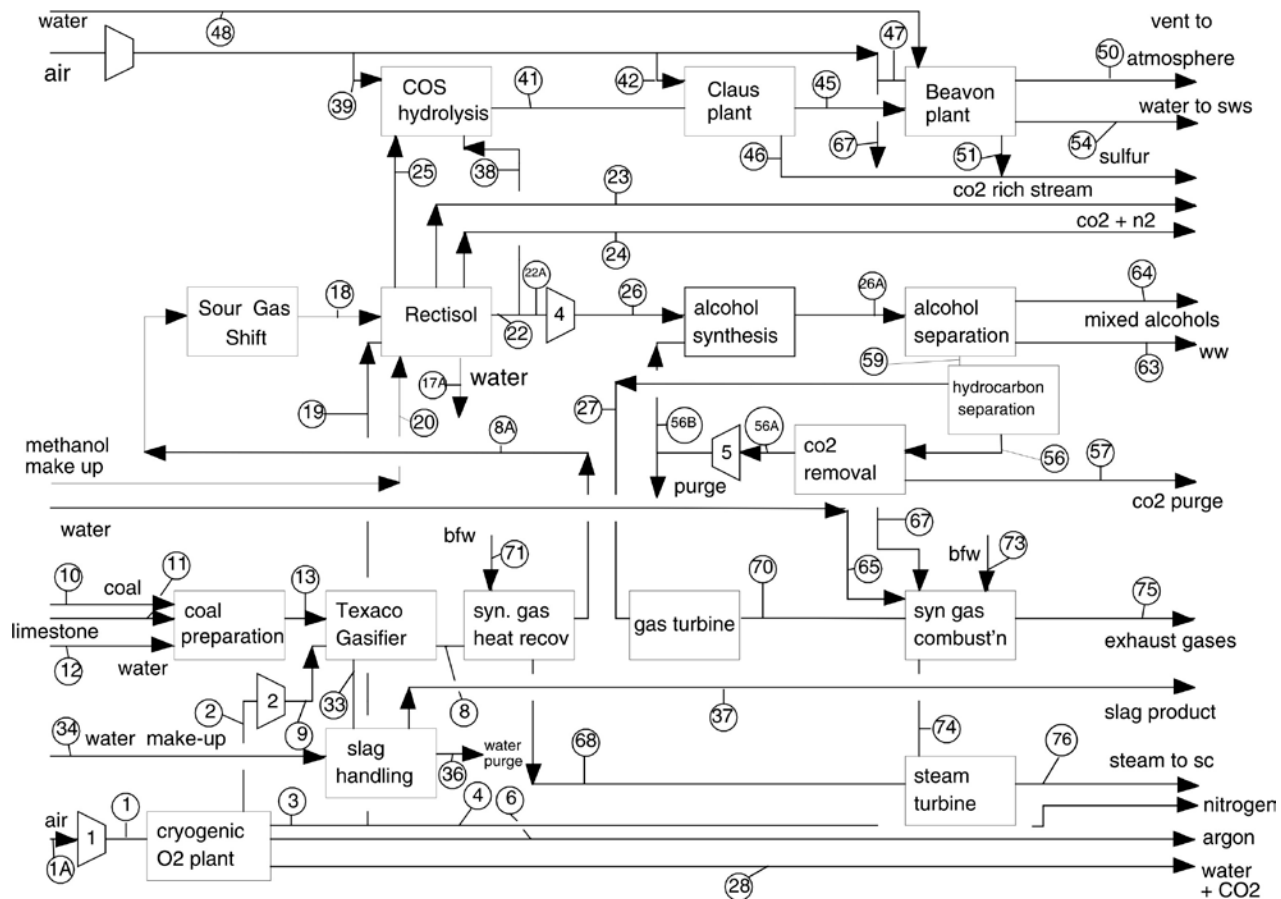


Figure 1.2: Block Flow Plant Diagram of a Coal to Higher Alcohol Fuels Process

# The Process Flow Diagram (PFD)

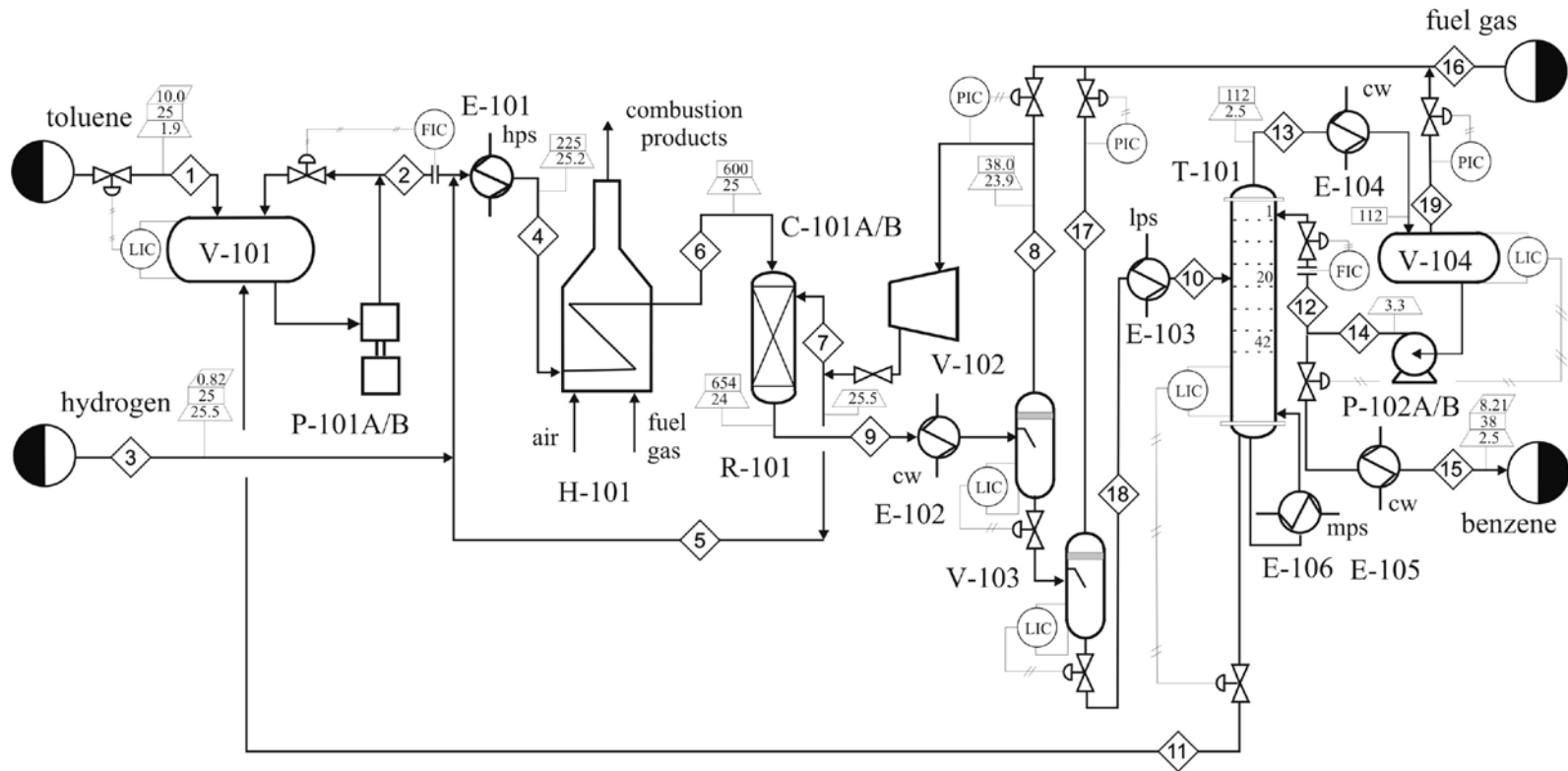
- PFD shows all process engineering information
- Typical conventions (vary by company):
  - All major equipment represented, uniquely numbered
  - All process flow streams shown and uniquely numbered, with description of thermodynamic conditions and composition (often in an accompanying table)
  - All utility streams supplied to major process equipment shown
  - Basic control loops, illustrating control strategy during normal operation

# The Process Flow Diagram (cont'd)

- The topology of the process – showing the connectivity of all the streams and the equipment
  - Example for toluene HDA – Figures 1.3 and 1.5
  - Tables 1.2 and 1.4 – list information that should be on the PFD but cannot fit
  - Use appropriate conventions – consistency is important in communication of process information
  - ex. Table 1.2

# Process Flow Diagram (cont'd)

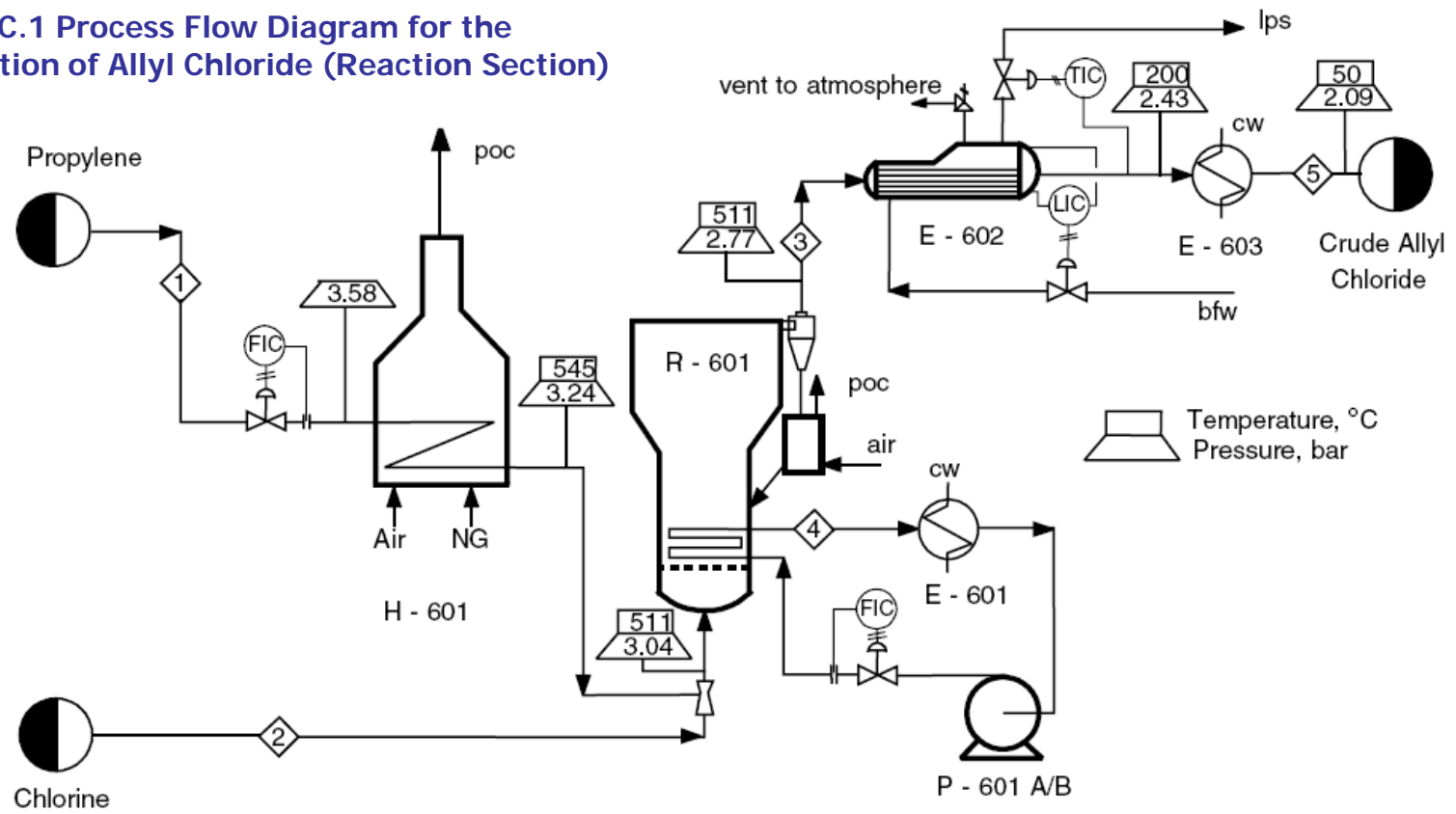
V-101	P-101A/B	E-101	H-101	R-101	C-101 A/B	E-102	V-102	V-104	E-103	E-106	T-101	E-104	V-103	P-102A/B	E-105
Toluene Storage Drum	Toluene Feed Pumps	Feed Preheater	Feed Heater	Reactor	Recycle Gas Compressor	Reactor Effluent Cooler	HighPres Phase Sep.	Low Pres. Phase Sep.	Tower Feed Heater	Benzene Reboiler	Benzene Column	Benzene Condenser	Reflux Drum	Reflux Pumps	Product Cooler



# Process Flow Diagram (cont'd)

H-601	R-601	J-601	E-601	P-601 A/B	E-602	E-603
Reactor Feed Heater	Fluidized Bed Reactor	Jet Mixer	Dowtherm Cooler	Dowtherm Pumps	Waste Heat Boiler	CrudeAllyl Chloride Cooler

Figure C.1 Process Flow Diagram for the Production of Allyl Chloride (Reaction Section)

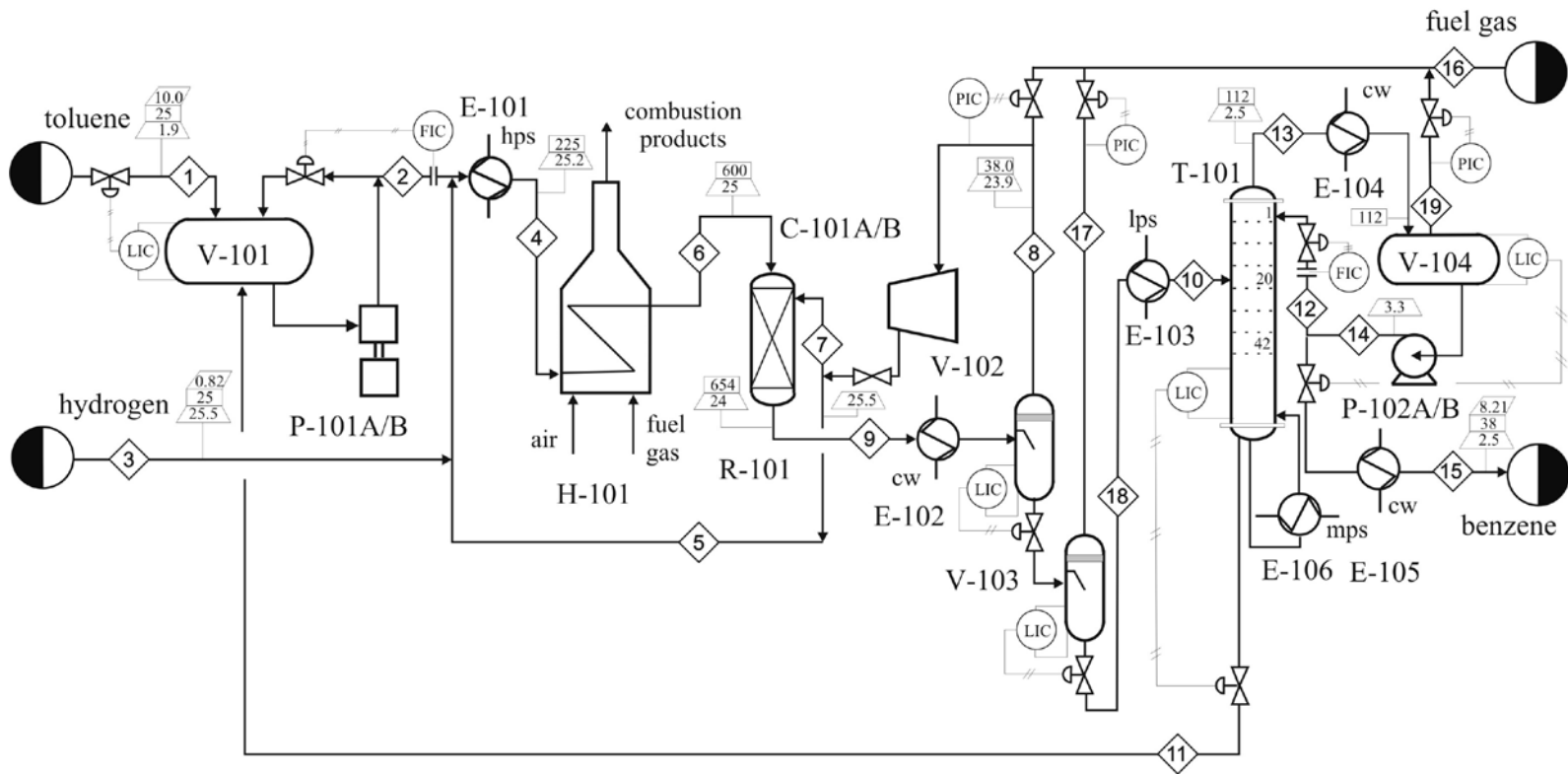


# Equipment Numbering

- *XX*-*YZZ* *A/B/...*
  - *XX* represents a 1- or 2-letter designation for the equipment (P = pump)
  - *Y* is the 1 or 2 digit unit number (1-99)
  - *ZZ* designates equipment number of unit (1-99)
  - *A/B/...* represents presence of spare equipment

# Equipment Numbering (cont'd)

V-101	P-101A/B	E-101	H-101	R-101	C-101 A/B	E-102	V-102	V-104	E-103	E-106	T-101	E-104	V-103	P-102A/B	E-105
Toluene Storage Drum	Toluene Feed Pumps	Feed Preheater	Feed Heater	Reactor	Recycle Gas Compressor	Reactor Effluent Cooler	HighPres Phase Sep.	Low Pres. Phase Sep.	Tower Feed Heater	Benzene Reboiler	Benzene Column	Benzene Condenser	Reflux Drum	Reflux Pumps	Product Cooler





# Equipment Numbering (cont'd)

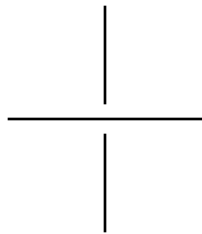
- T-905 is the 5th tower in unit nine hundred
- P-301 A/B is the 1st Pump in unit three hundred plus a spare

# Equipment Numbering (cont'd)

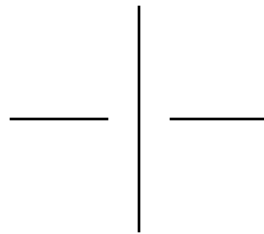
- Use unambiguous letters for new equipment
  - Ex. Turbine use Tb or J not T (used for tower)
  - Replace old vessel V-302 with a new one of different design - use V-319 (e.g.) not V-302 – since it may be confused with original V-302

# Stream Numbering & Drawing

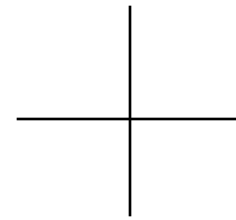
- Number streams left to right when possible
- Horizontal lines are dominant



yes



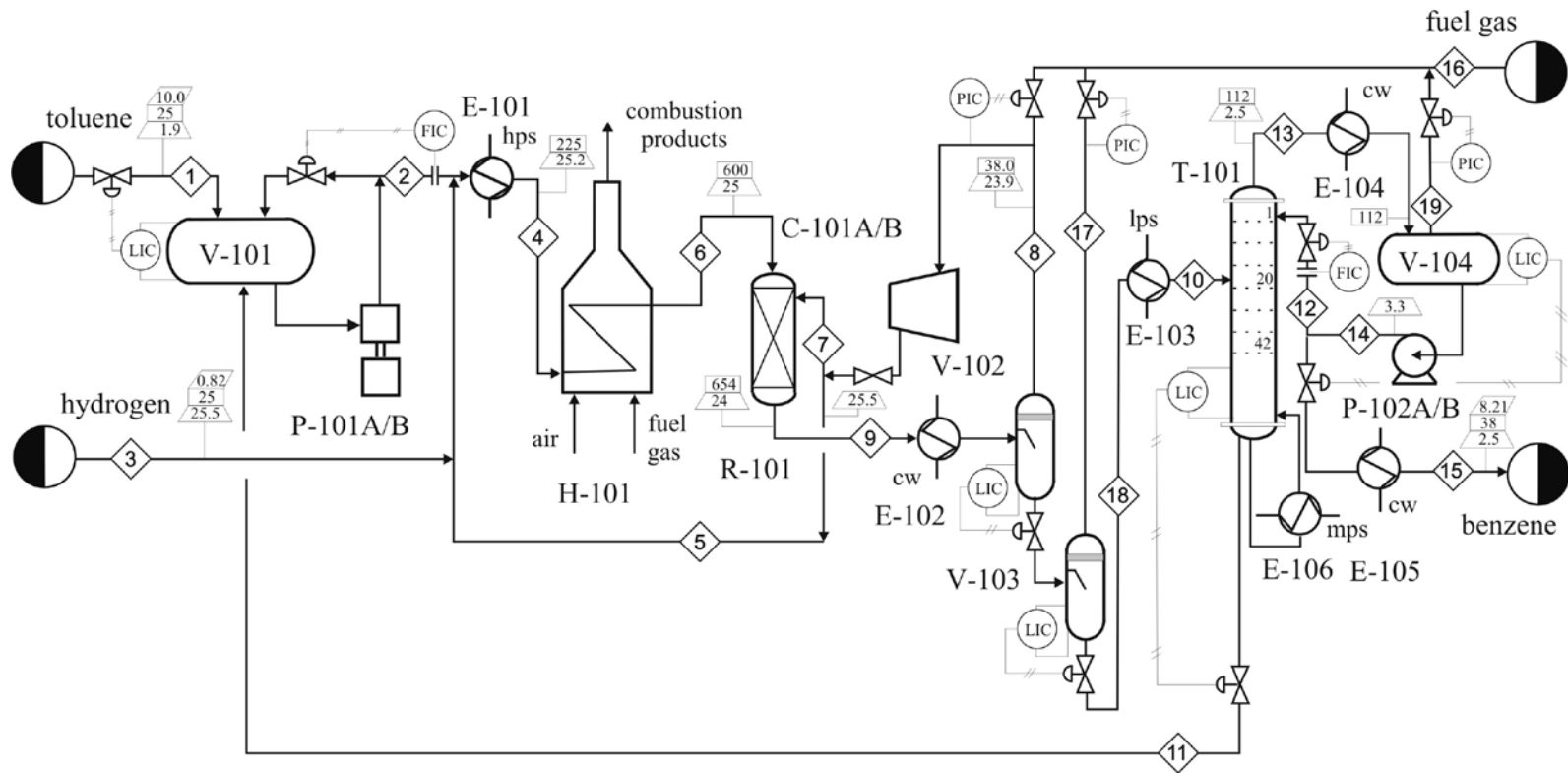
no



no

# Stream Numbering & Drawing (cont'd)

V-101	P-101A/B	E-101	H-101	R-101	C-101 A/B	E-102	V-102	V-104	E-103	E-106	T-101	E-104	V-103	P-102A/B	E-105
Toluene Storage Drum	Toluene Feed Pumps	Feed Preheater	Feed Heater	Reactor	Recycle Gas Compressor	Reactor Effluent Cooler	HighPres Phase Sep.	Low Pres. Phase Sep.	Tower Feed Heater	Benzene Reboiler	Benzene Column	Benzene Condenser	Reflux Drum	Reflux Pumps	Product Cooler



# Stream Numbering & Drawing (cont'd)

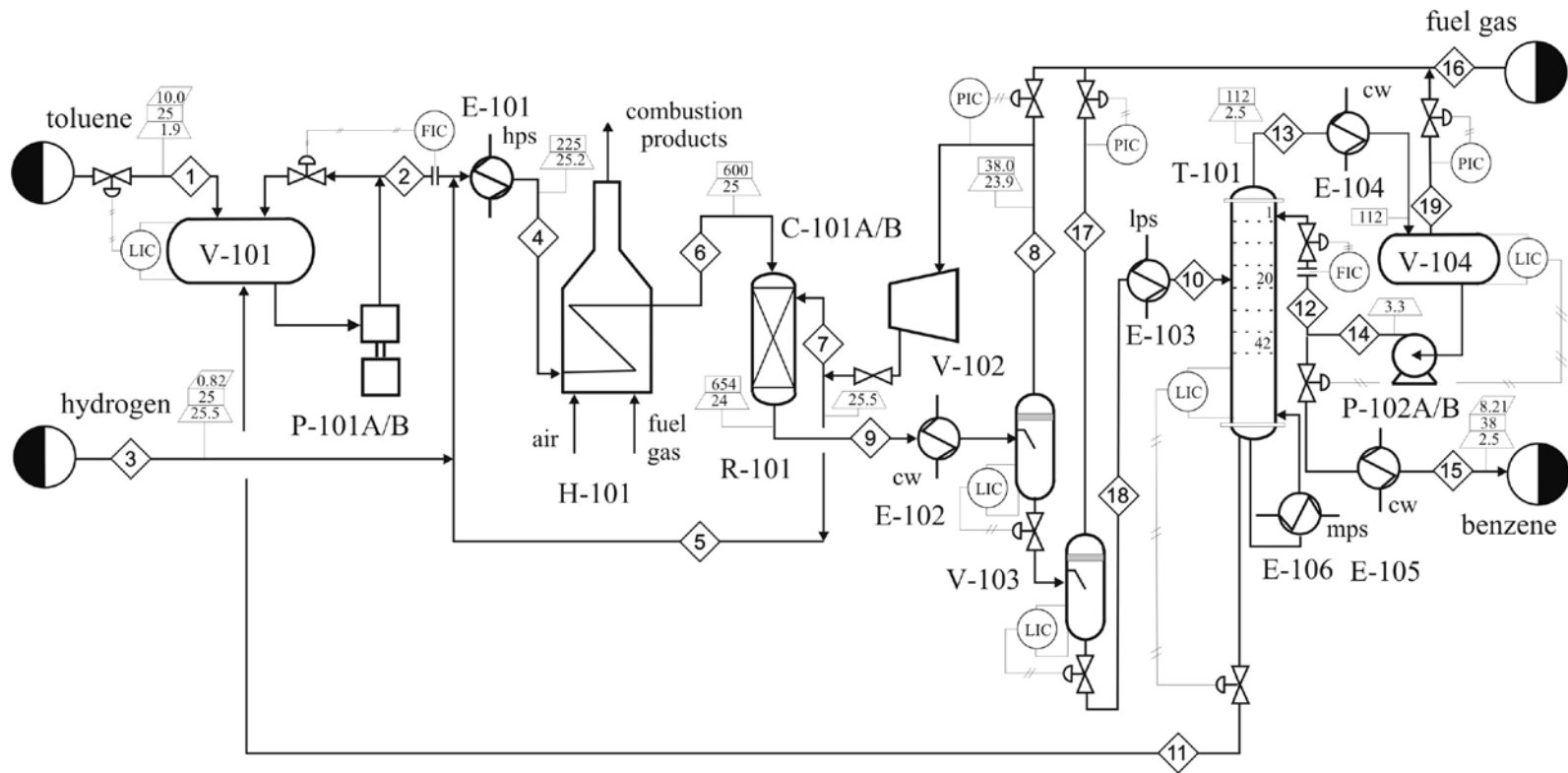
- Add arrows for
  - change in direction
  - inlet of equipment
  
- Utility streams
  - use convention in Table 1.3
  - lps, cw, fg, etc.

# Stream Information

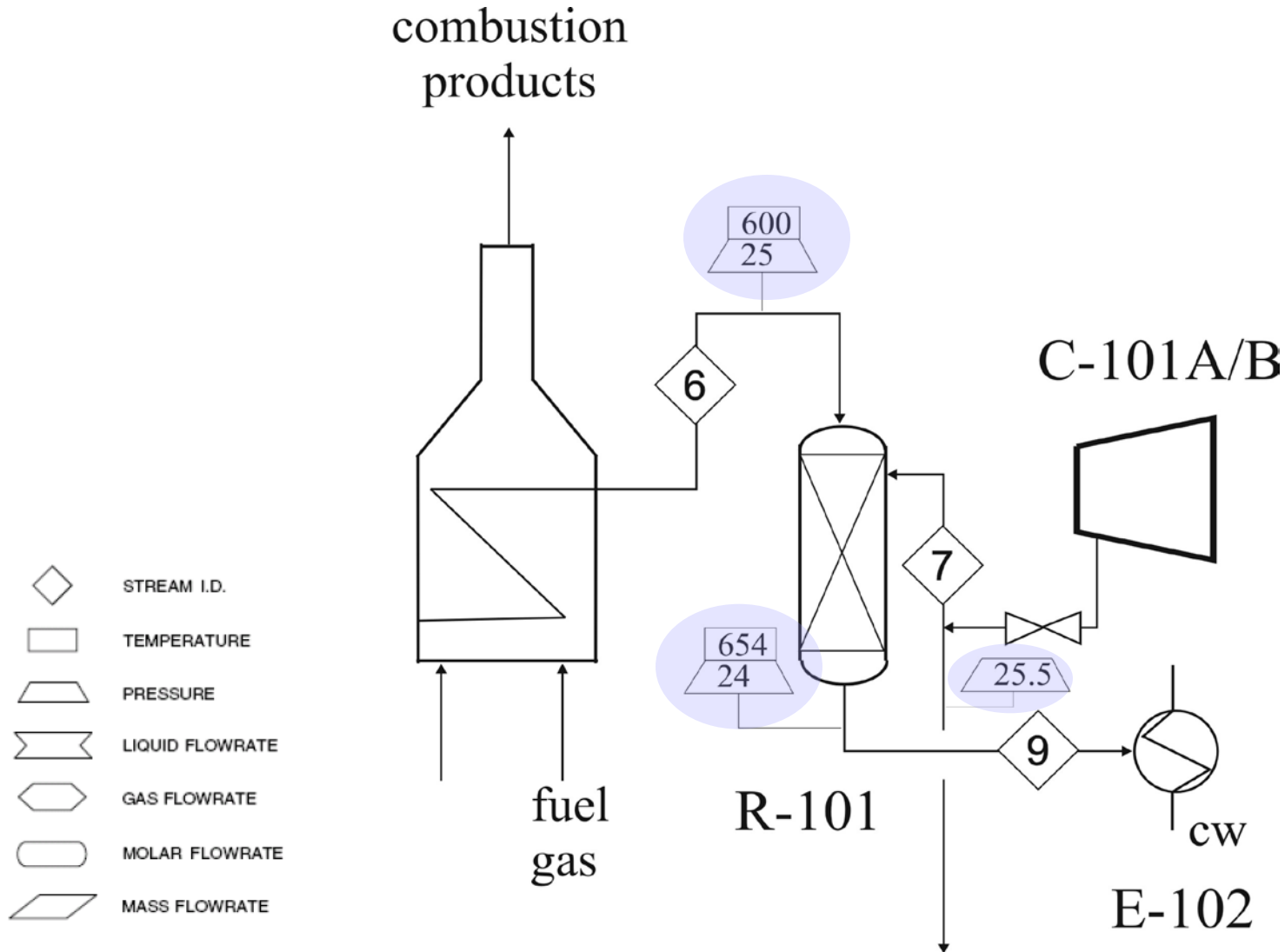
- Since diagrams are small, not much stream information can be included
- Include important data – around reactors and towers, etc.
  - Flags are used – see toluene HDA diagram
  - Full stream data, as indicated in Table 1.4, are included in a separate flow summary table – see Table 1.5

# Stream Numbering & Drawing (cont'd)

V-101	P-101A/B	E-101	H-101	R-101	C-101 A/B	E-102	V-102	V-104	E-103	E-106	T-101	E-104	V-103	P-102A/B	E-105
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# Stream Information - Flags





# Stream Drawing

Future Equipment	-----
Major Process	—————
Minor Process	—————
Pneumatic	——#——#——#——#——
Hydraulic	——L——L——L——
Capillary Tubing	——X——X——X——X——
Mechanical Link	——●——●——●——●——

# Stream Drawing

Electromagnetic, Sonic

Optical, Nuclear

Electric

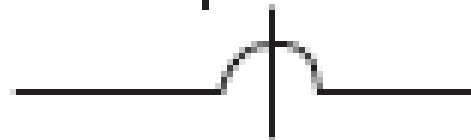
Connecting Line

Non-Connecting Line

Non-Connecting Line

Jacketed or Double Containment

Software or Data Link



# The Process Flow Diagram (cont'd)

## Essential Information

Stream Number  
Temperature ( $^{\circ}\text{C}$ )  
Pressure (bar)  
Vapor Fraction  
Total Mass Flow Rate (kg/h)  
Total Mole Flow Rate (kmol/h)  
Individual Component Flow Rates (kmol/h)

## Optional Information

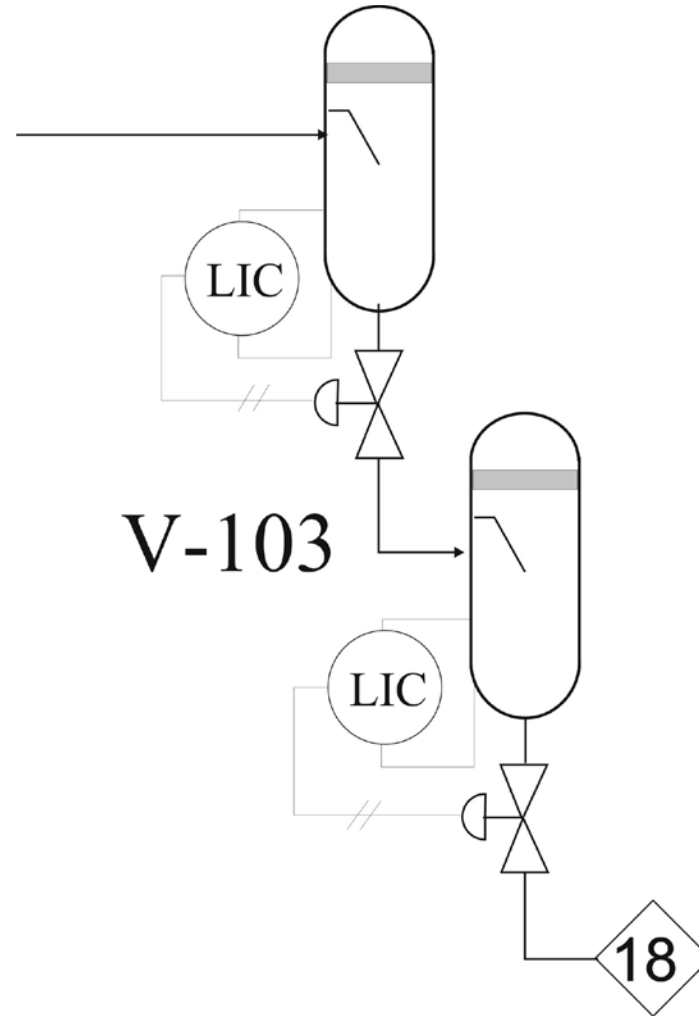
Component Mole Fractions  
Component Mass Fractions  
Individual Component Flow Rates (kg/h)  
Volumetric Flow Rates ( $\text{m}^3/\text{h}$ )  
Significant Physical Properties  
    Density  
    Viscosity  
    Other  
Thermodynamic Data  
Heat Capacity  
Stream Enthalpy  
K-values  
Stream Name

Table 1.4: Information  
in a Flow Summary

# Basic Control Loops

- Often the basic control loops (those involving maintaining material balance and reactor controls) are included on the PFD; instrumentation and other control loops are not shown
- The final control element in nearly all chemical process control loops is a valve.

# Basic Control Loops



# Basic Instrumentation Symbols

